

Dynamic Modeling of Advanced Process Configurations for Post- Combustion Amine Scrubbing

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**Texas Carbon Management Program
University of Texas at Austin**



Challenges for CCS

Energy Penalty

~20-30% reduction in power plant output

Capital Cost

800 MW coal plant: > 3 billion ft³/day flue gas



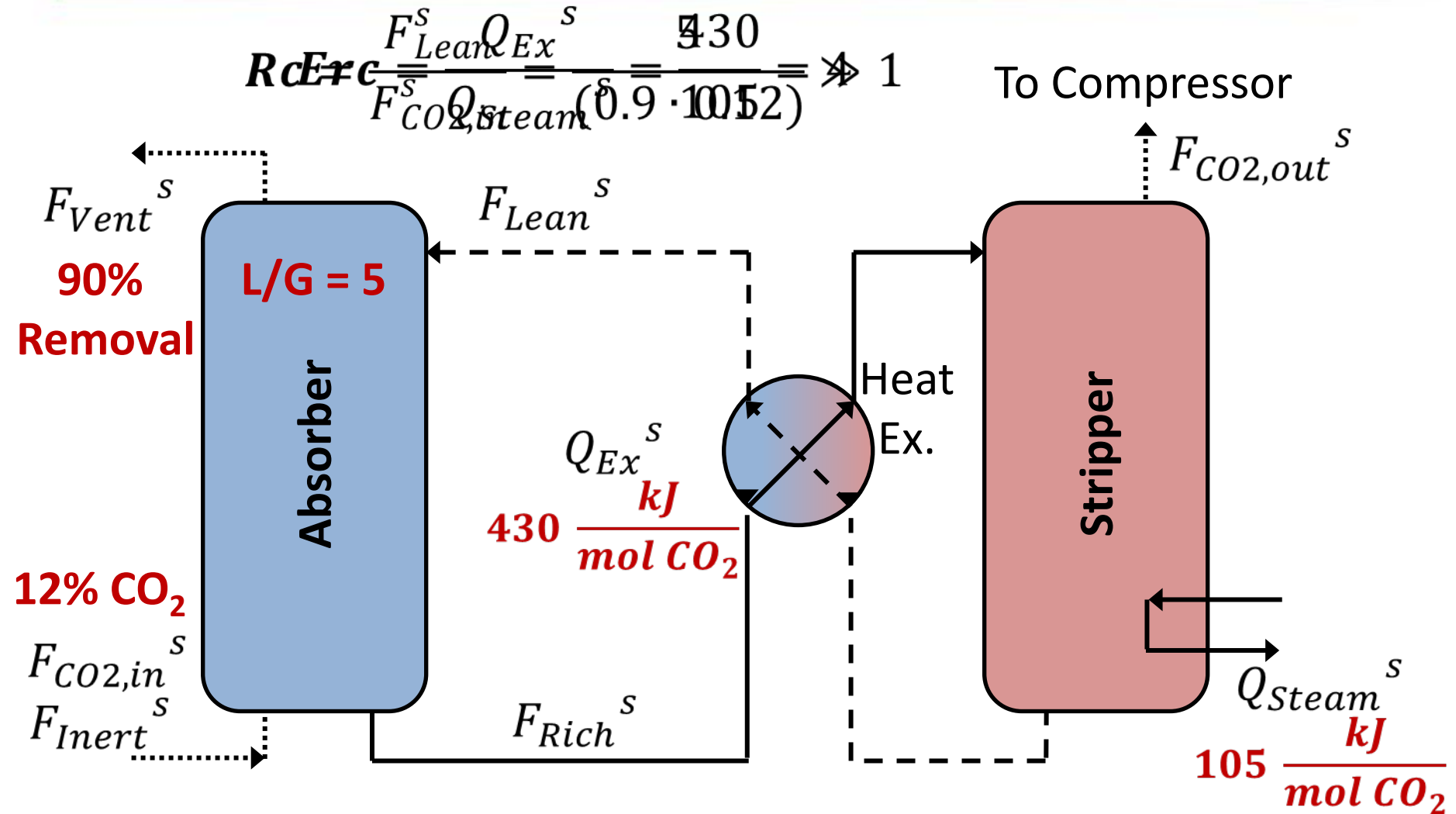
Tight Integration

High material and energy recycle

Minimization of equipment size and solvent inventory



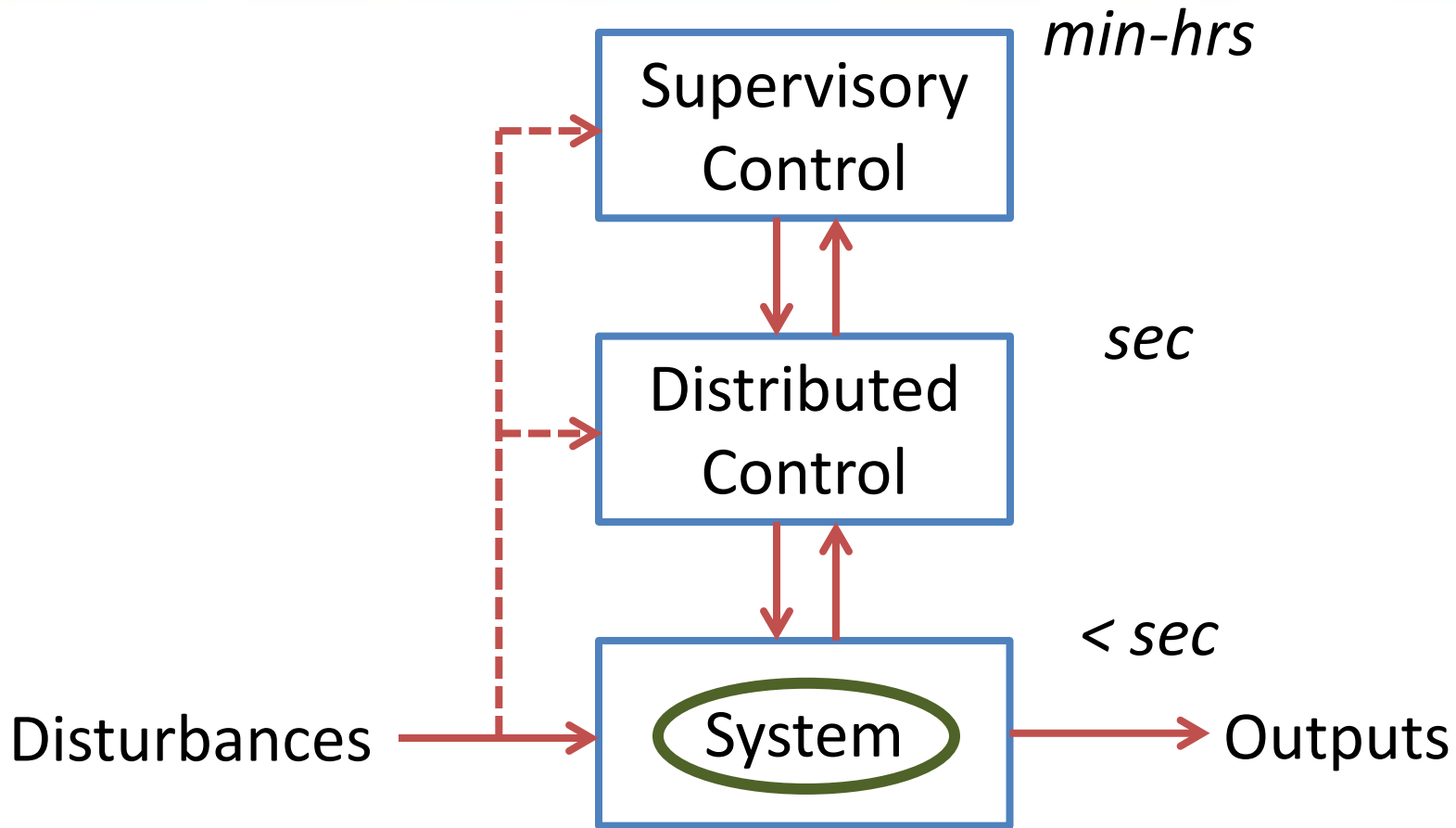
Heavy Material and Energy Recycle



Baldea, M., Daoutidis, P. (2012). *Dynamics and Nonlinear Control of Integrated Process Systems*.



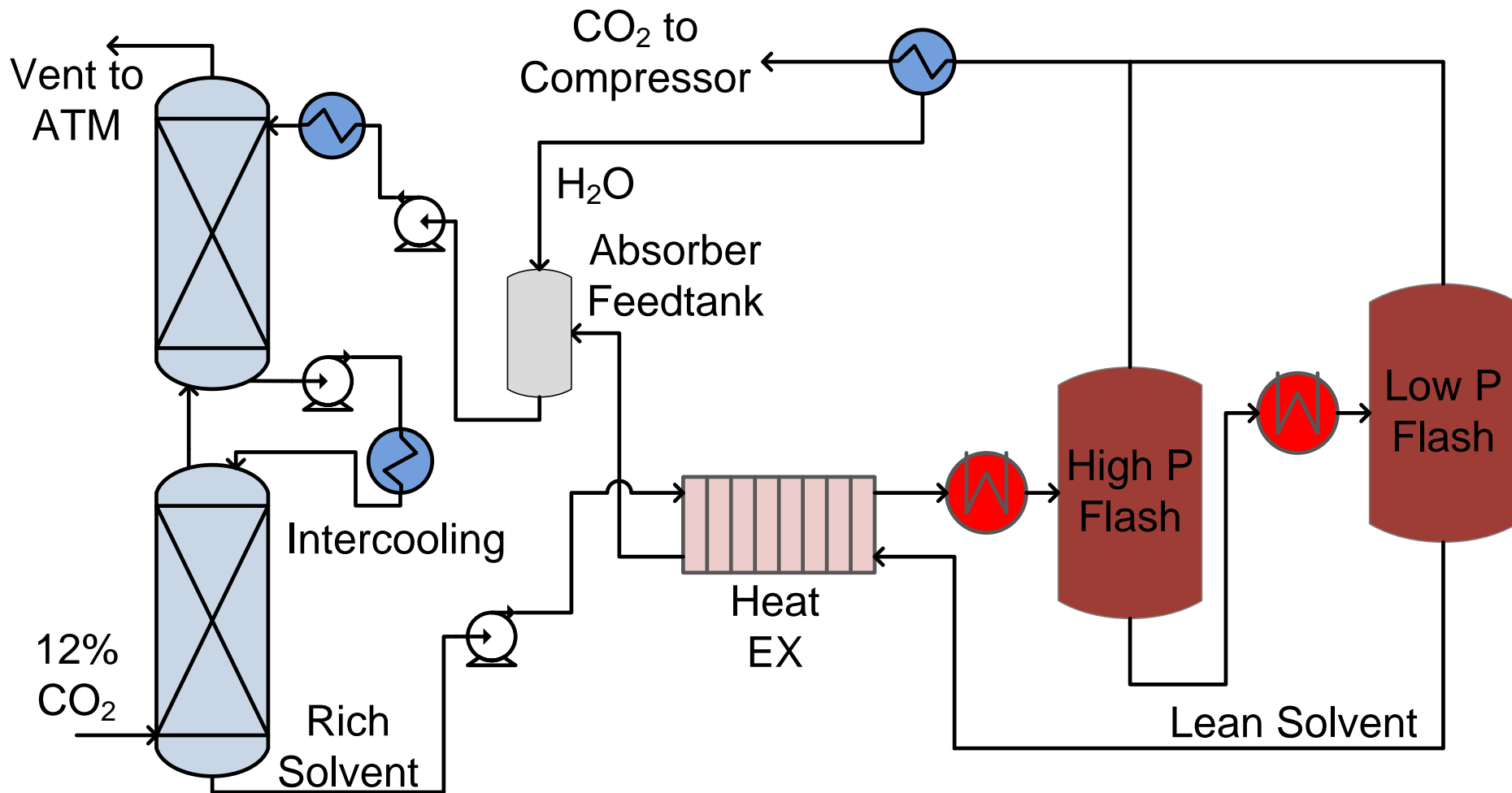
Hierarchical Controller Design



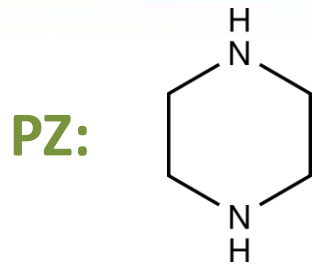
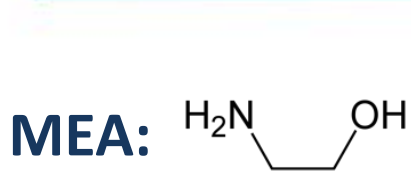
Goal: Develop dynamic model for control strategy design



Process Modeling: Advanced Configuration



Process Modeling: Advanced Solvent



Previous Works



This Research



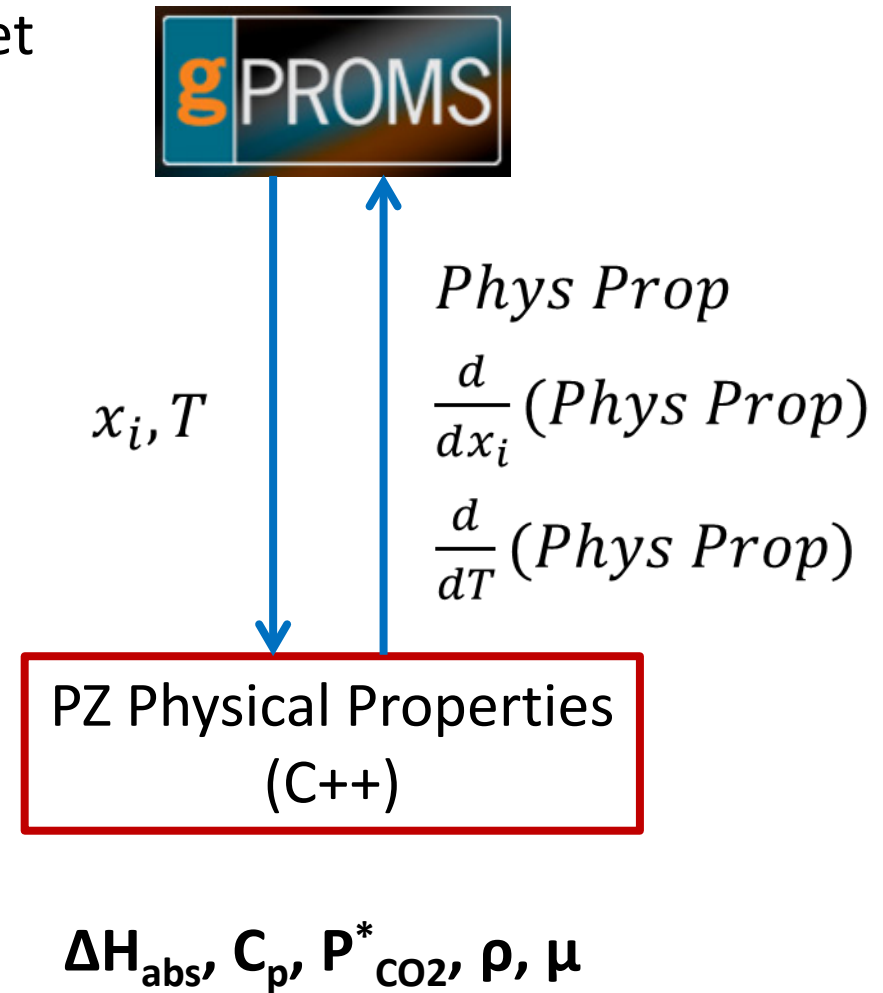
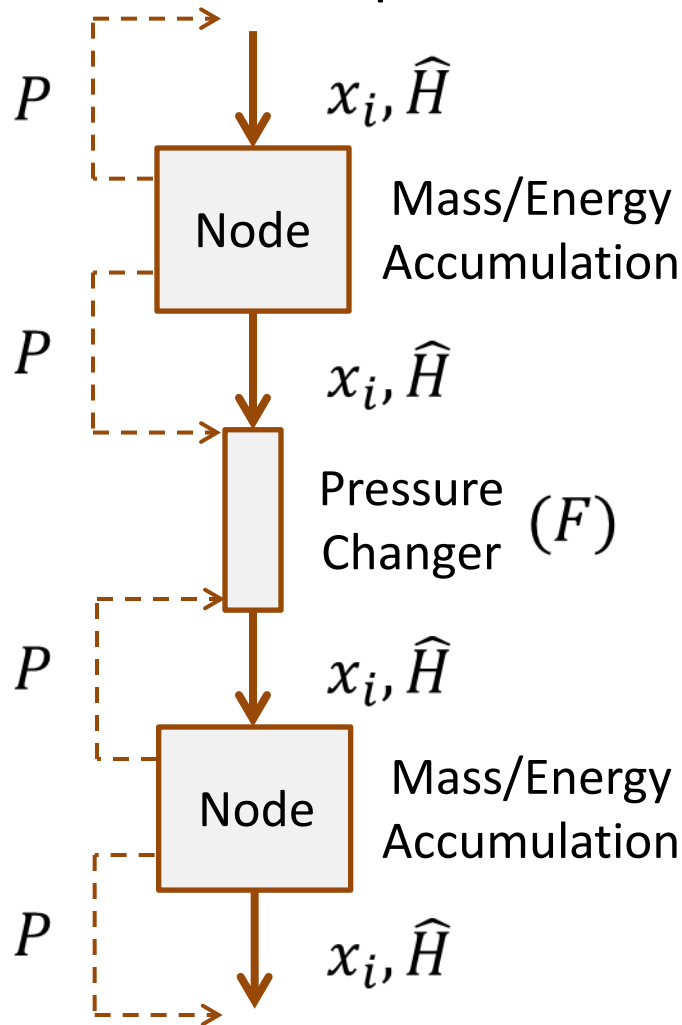
Property	7 m MEA	8 m PZ
$k_g' \times 10^7$ (mol/Pa·s·m ²)	4.3	8.5
Capacity (mol CO ₂ /mol PZ + H ₂ O)	0.67	0.88
Degradation T (°C)	121	163
Max stripper P (bar)	4	16
Degradation rate at 120°C (1/week)	8.1%	0.07%
C _{amine} in gas at 40°C (ppm)	13	8
ΔH_{abs} at lean ldg (kJ/mol CO ₂)	-76	-71

Rochelle et al. (2011). *Chem Eng*, 171(3), 725-733.



Modeling Software: gPROMS[©]

Equation-oriented process flowsheet



Model Validation: SRP Pilot Plant

Stripper



Absorber

**Two-Stage
Flash**

Validation Data:

Fall 2011

PZ Solvent

Two-Stage Flash

Stripper

Intercooled

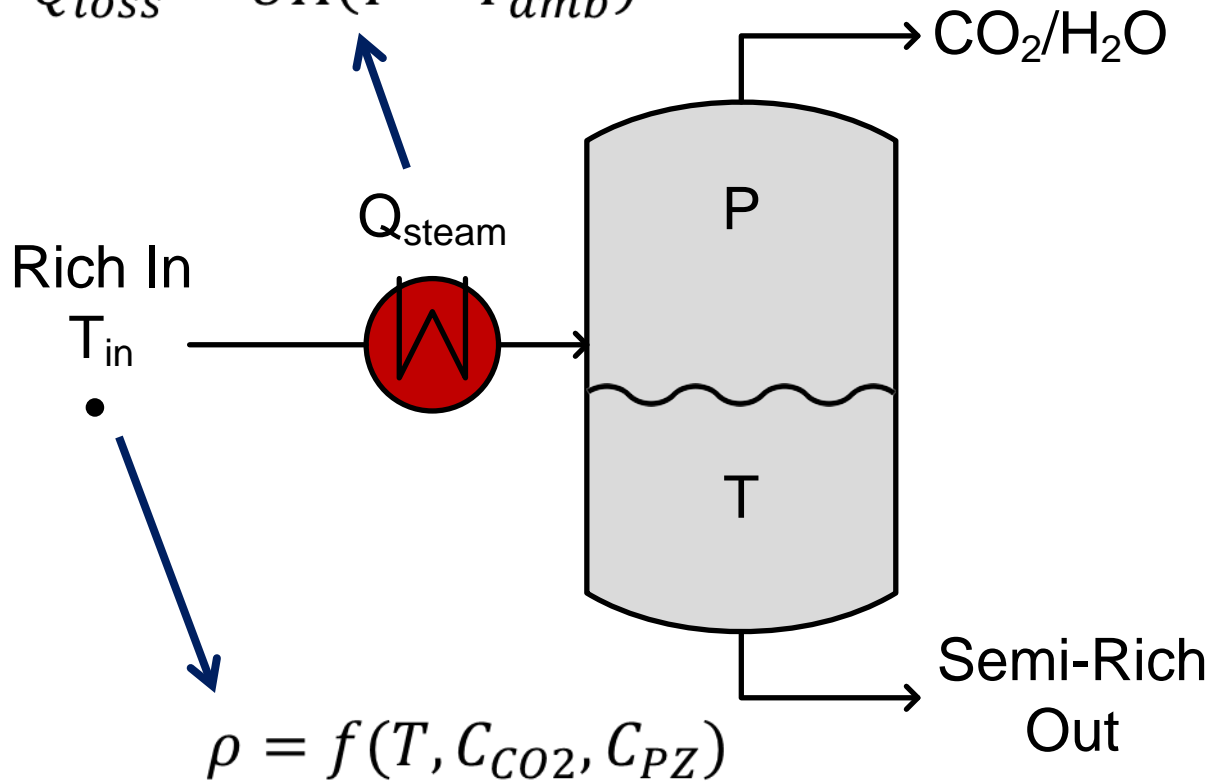
Absorber



Flash Tank Model

$$Q_{eff} = Q_{steam} - Q_{loss}$$

$$Q_{loss} = UA(T - T_{amb})$$



$$\rho = f(T, C_{CO_2}, C_{PZ})$$

$$\frac{\rho}{\rho_{H_2O}} = \left(\frac{\rho}{\rho_{H_2O}}\right)_{meas} + \left(\frac{\rho}{\rho_{H_2O}}\right)_{bias}$$

Fitted:

$$\left(\frac{\rho}{\rho_{H_2O}}\right)_{bias} = 0.0082$$

~4% Increase in
experimental loading

Fitted:

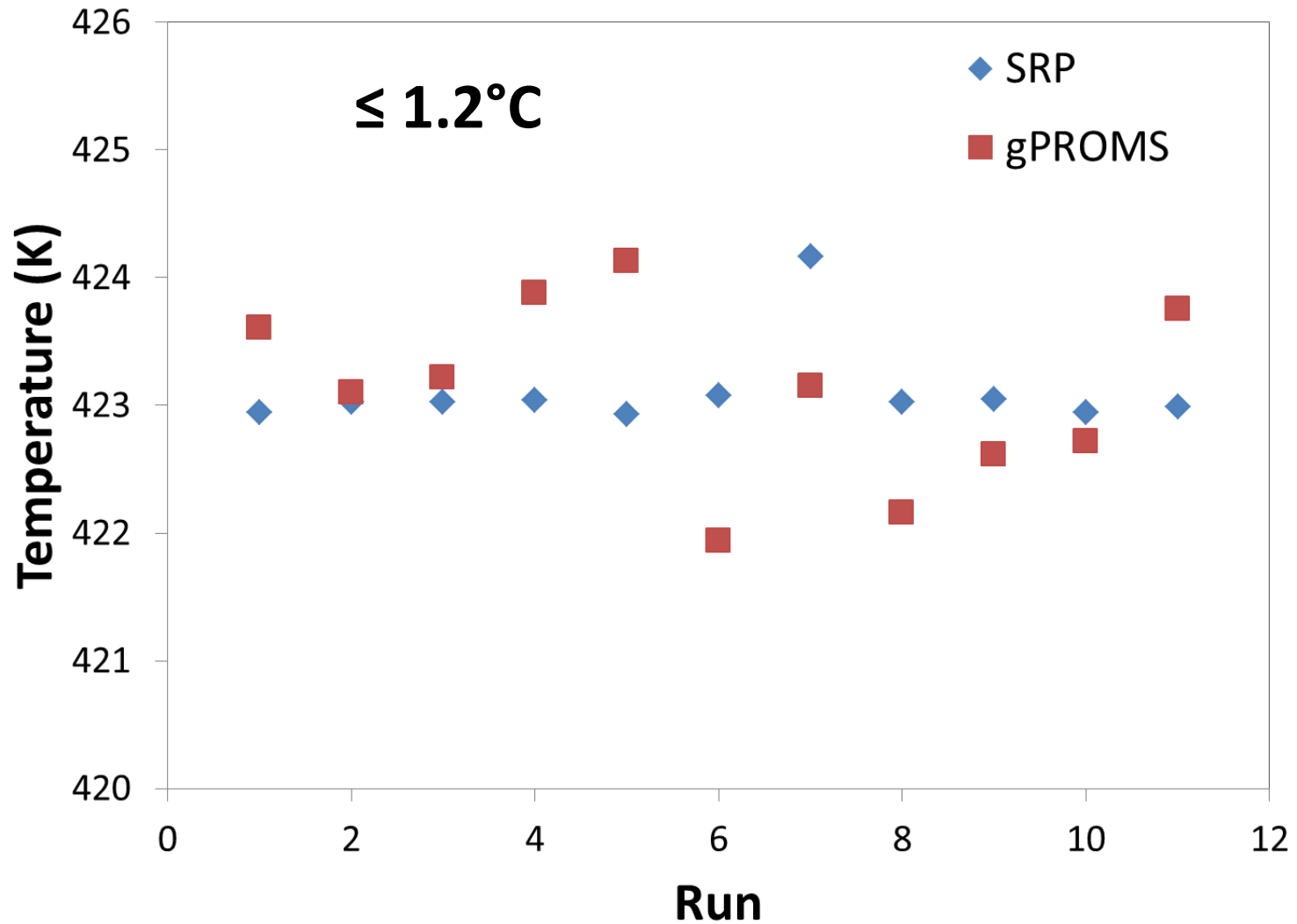
$$UA = 0.075 \text{ kW/K}$$

Experimental
(both tanks):

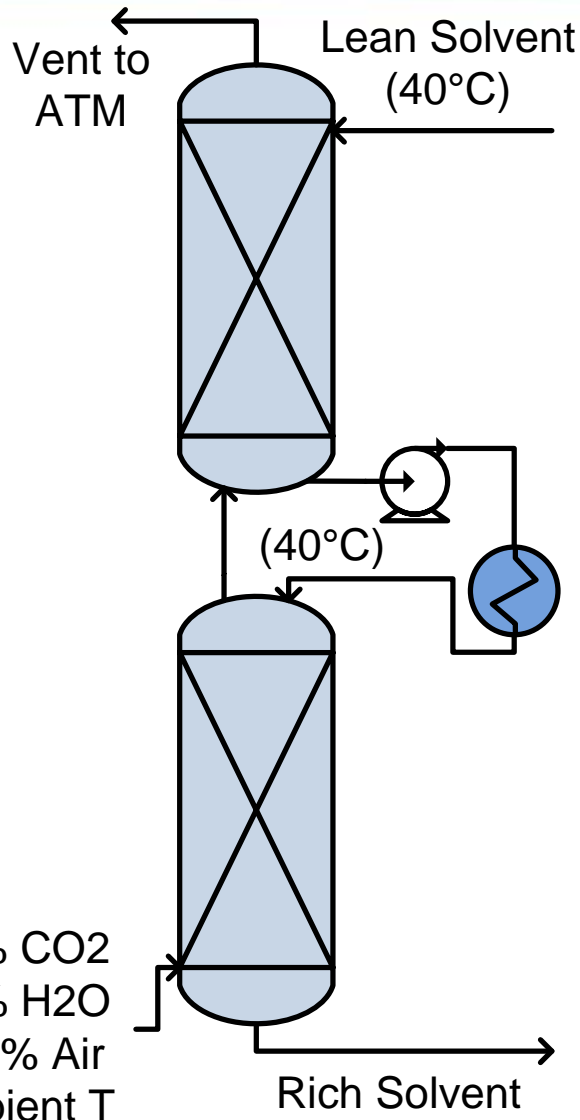
$$UA = 0.054 \text{ kW/K}$$



Steady State Flash Tank Validation



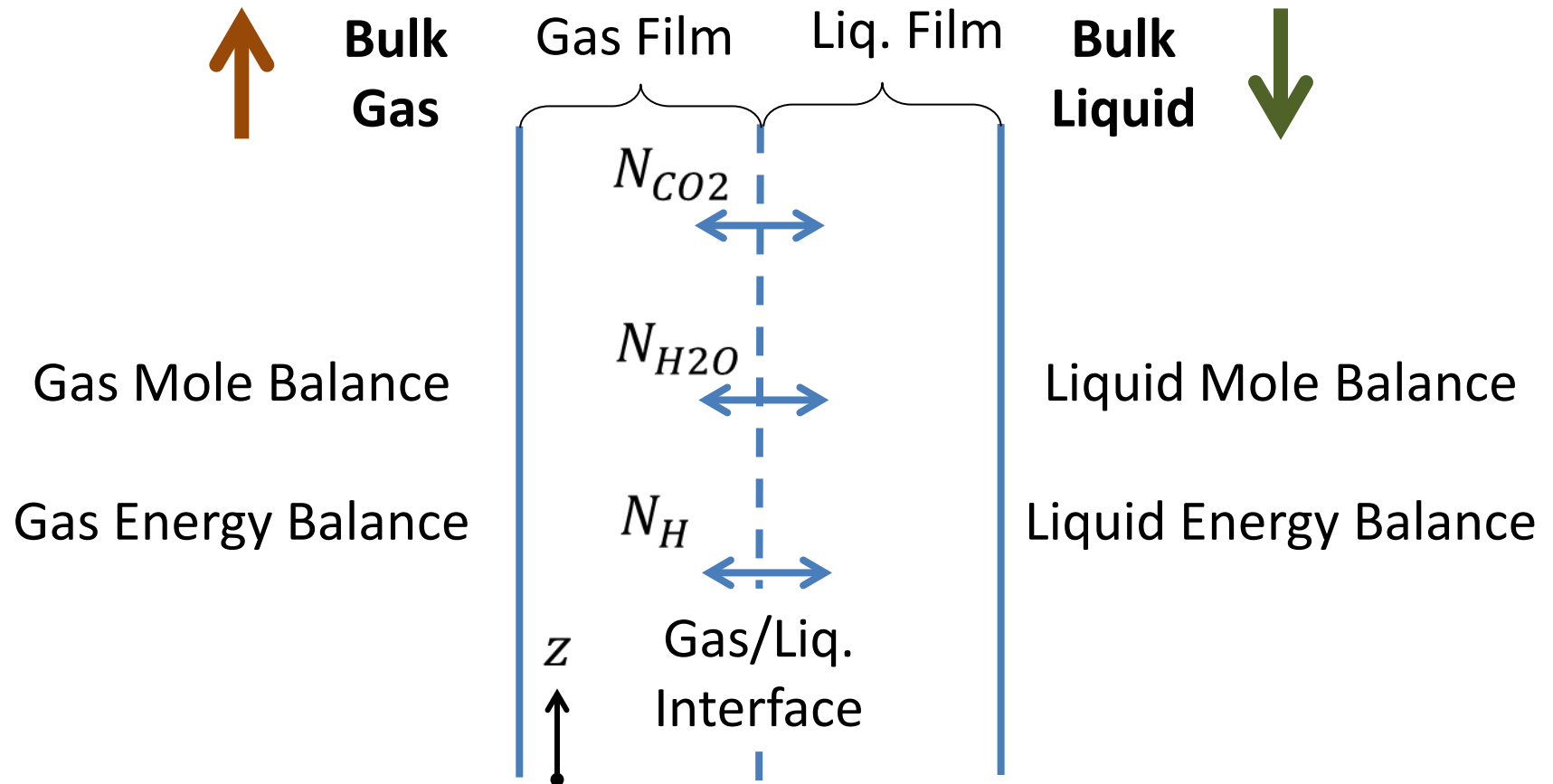
Intercooled Absorber Model



- Ideal gas law is valid
- PZ is nonvolatile
- Mass transfer of H₂O is gas film controlled
- Heat transfer is gas film controlled
- Equilibrium at the gas/liquid interface
- No accumulation at the gas/liquid interface
- Constant pressure drop
- Plug flow regime



Absorber Model Development



Absorber Mass Transfer

Liquid film:

$$k'_g = f(\alpha)$$

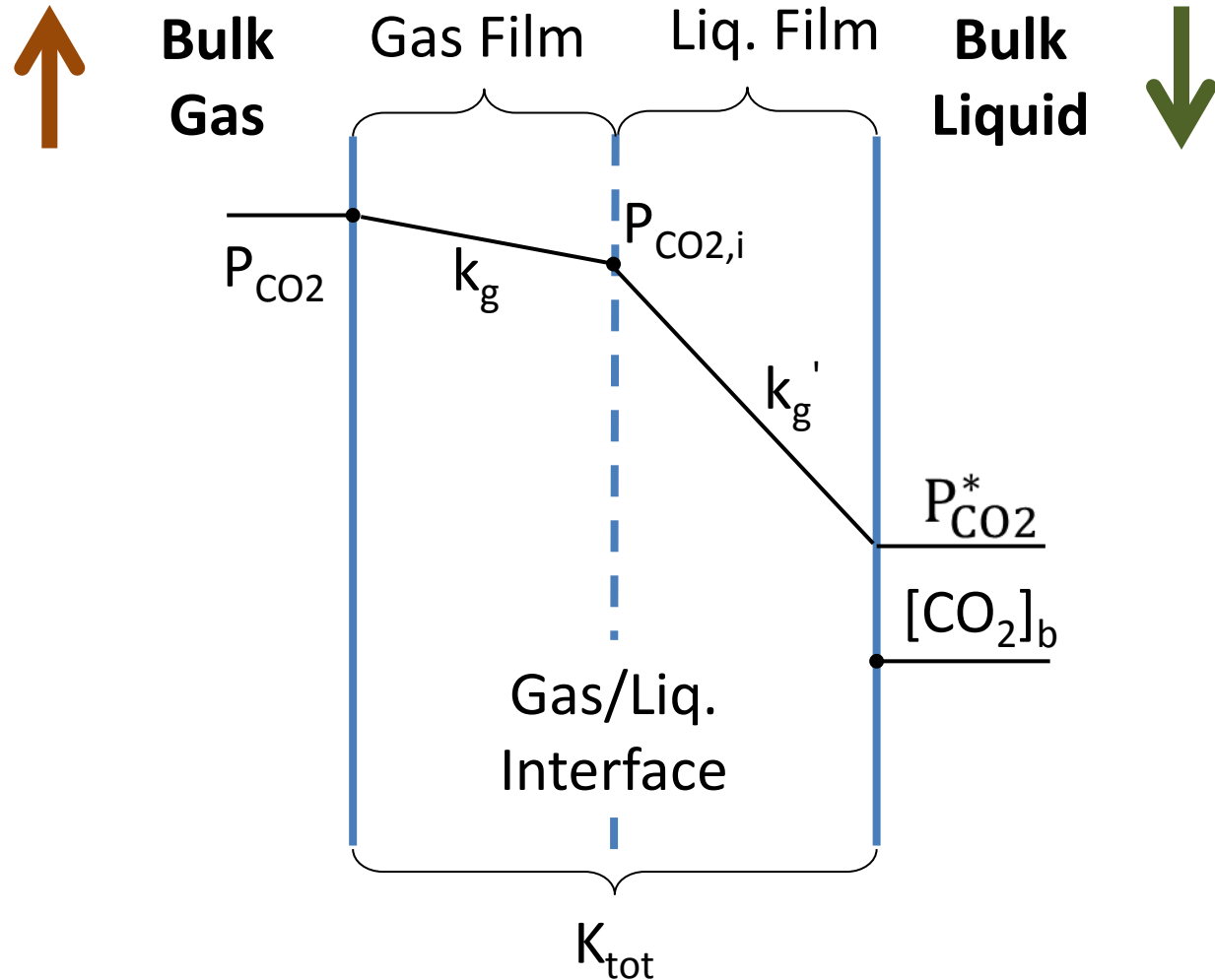
Overall Mass

Transfer Coefficient:

$$\frac{1}{K_{tot}} = \frac{1}{k_g} + \frac{1}{k'_g}$$

Rate-Based Flux:

$$N_{CO_2} = K_{tot}(P_{CO_2} - P_{CO_2}^*)$$



Wetted Wall Column Validation

Cooling Oil

$$T = \text{constant}$$
$$\frac{\partial E}{\partial t} = 0$$



$$\alpha_{\text{in}} \approx \alpha_{\text{out}}$$

$$\ln[P_{\text{CO}_2}^*] = f(\alpha, T)$$

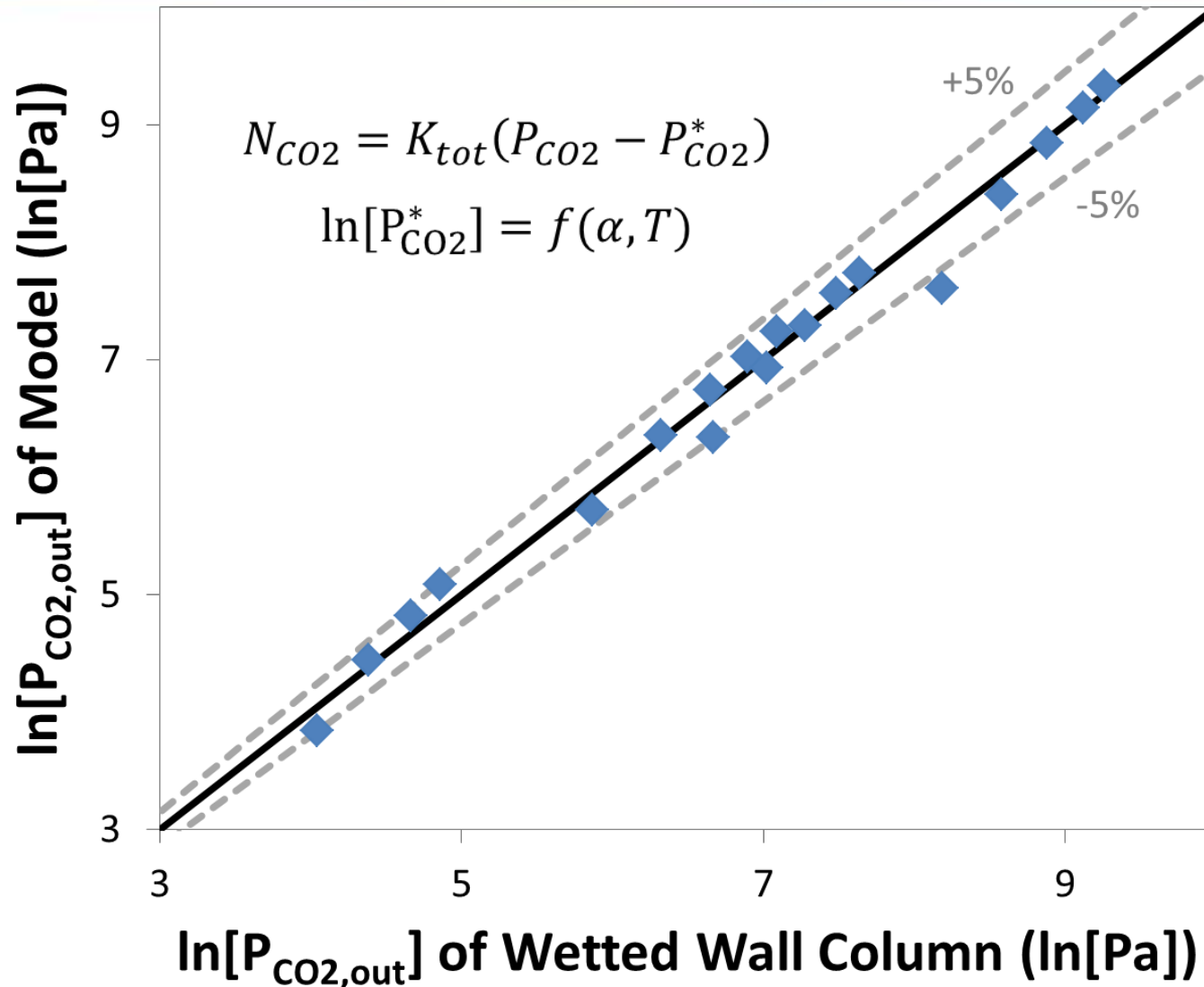
Given loading



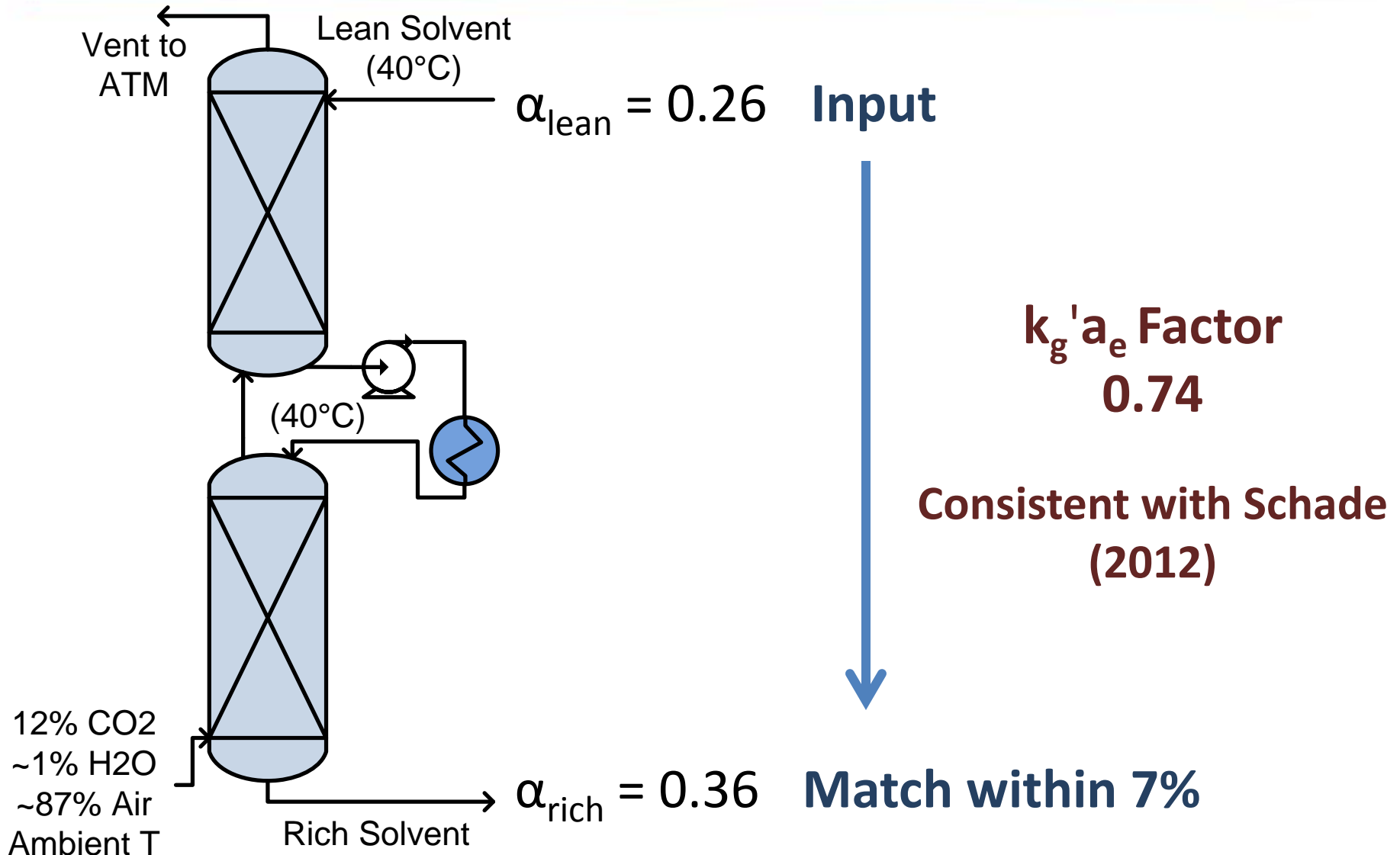
Predict Flux



Wetted Wall Column Validation Results



Steady State Absorber Validation



Mass Transfer Coefficient Uncertainty



Bulk Gas

Gas Film

Rxn Film
Diff Film

Bulk Liquid



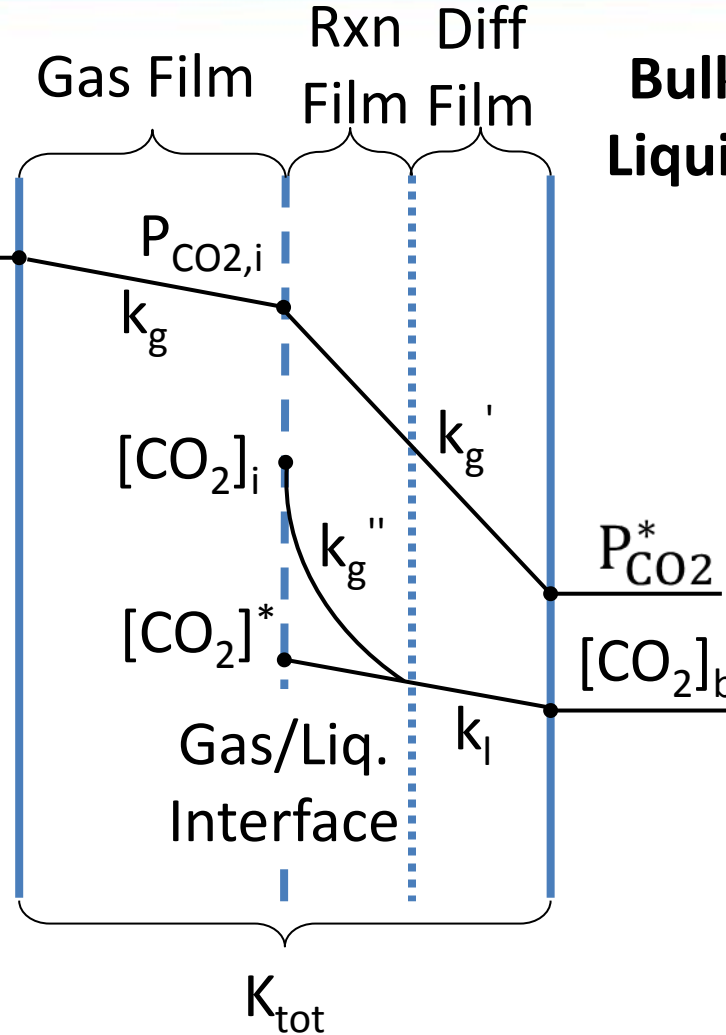
Empirical Correlation
Uncertainty

$$k'_g = -2.0 \times 10^{-5} \alpha + 8.2 \times 10^{-6}$$

$\pm 20\%$

$$\frac{a_e}{a_p} = 1.34 \left[(We) (Fr)^{-\frac{1}{3}} \right]^{0.116}$$

$\pm 13\%$



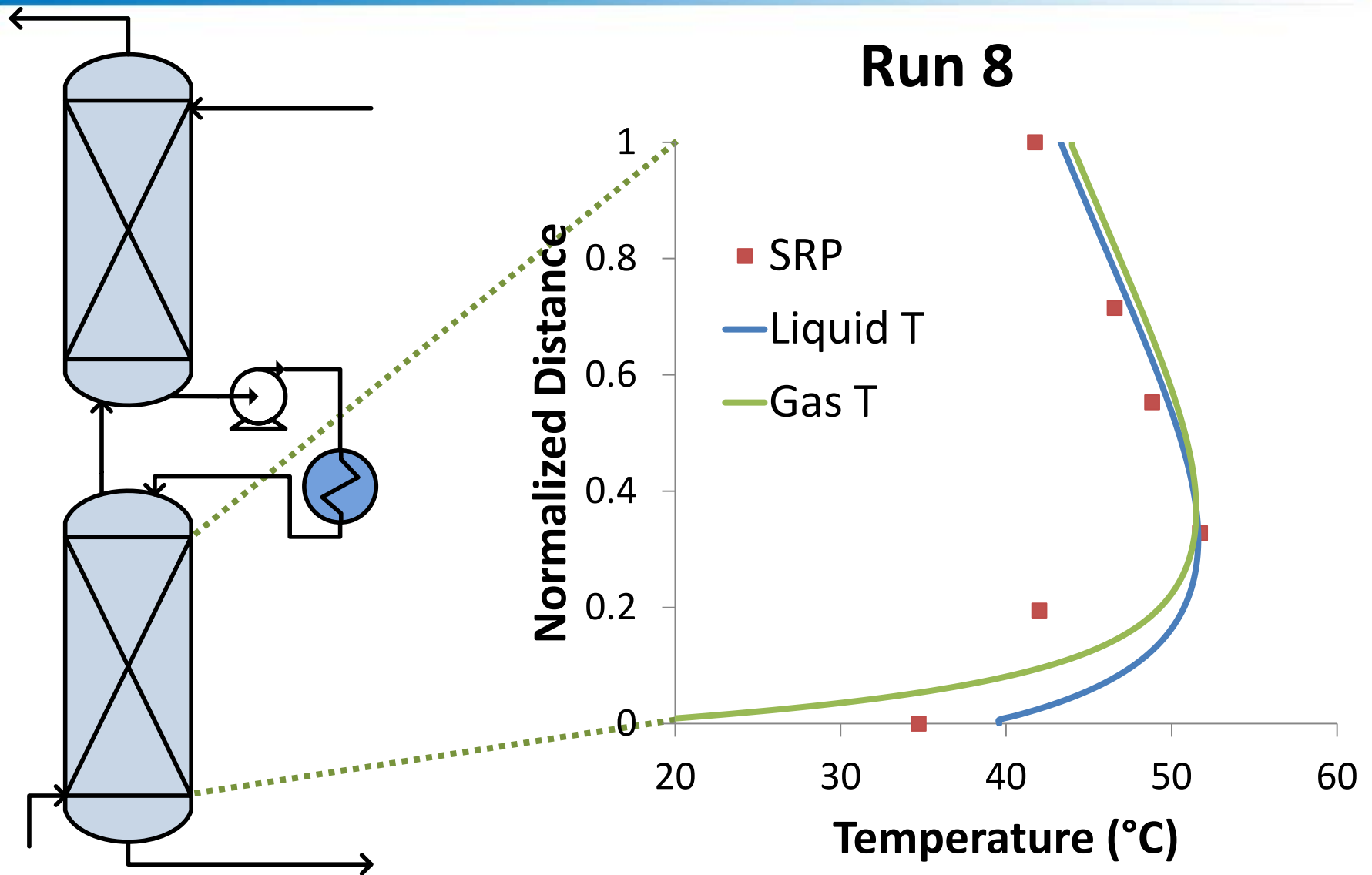
Liquid film mass transfer coefficient:

$$\frac{1}{k'_g} = \frac{m_{CO_2}}{k_l} + \frac{1}{k''_g}$$

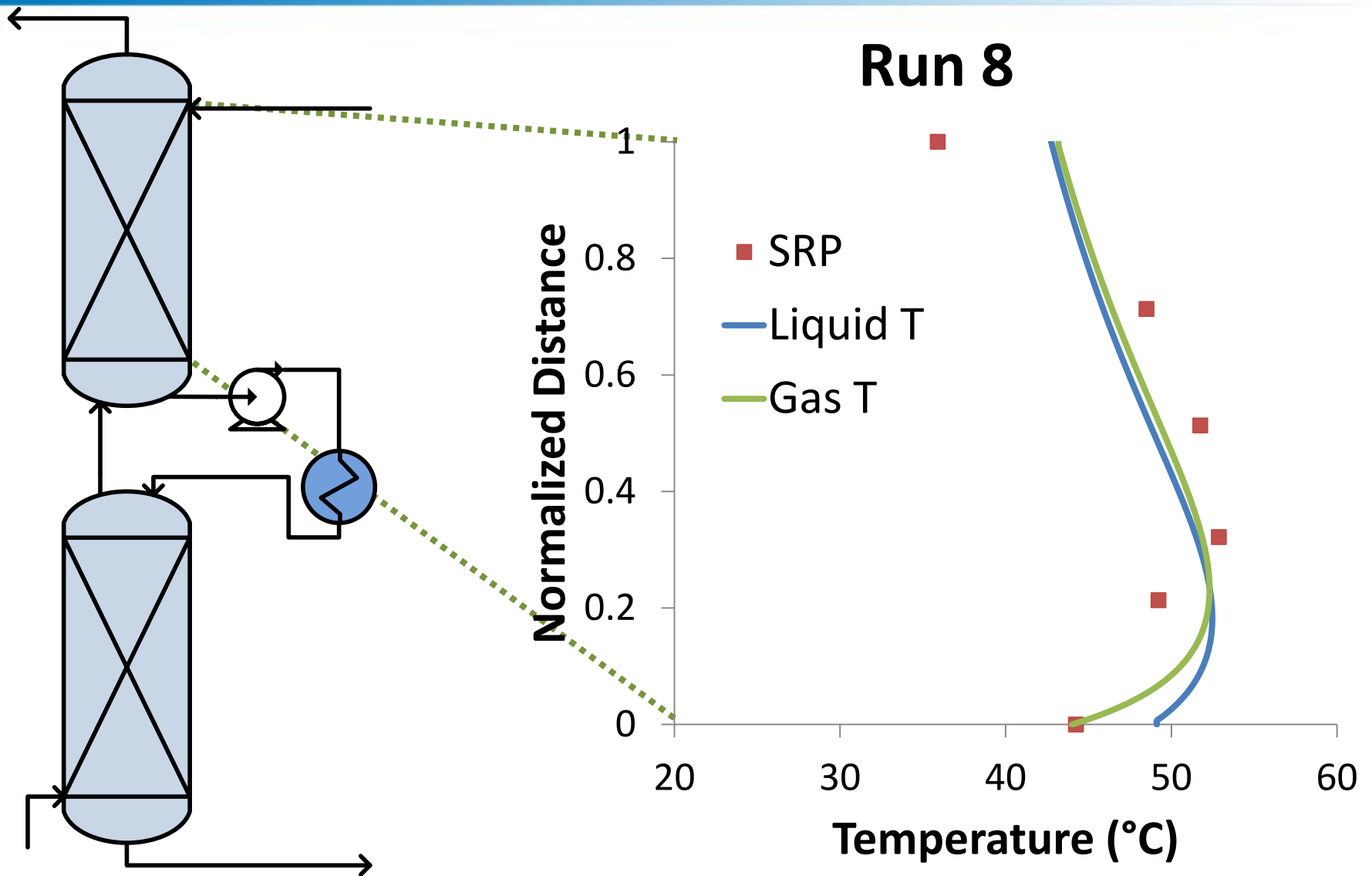
k''_g - Pseudo 1st order mass transfer coefficient



Steady State Absorber Validation



Steady State Absorber Validation



Conclusions

- Heavy energy and material recycle lead to multiple time scale behavior in the amine scrubbing system
- Flash tank temperature predicted within 1.2°C after adjusting loading by 4% heat loss by 40%
- Absorber with $k_g' = f(\alpha)$ predicts experimental $\ln[P_{CO_2}]$ for wetted wall column with average error of 2.2%
- Absorber loading matched within 7% with 26% decrease in $a_e k_g'$
- Behavior of absorber temperature profile consistent with pilot plant measurements



Questions?

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Titles and abstracts due October 15, 2013 to gtr@che.utexas.edu



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