

# Amine Solvent Reclaiming

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- Why is Amine Solvent Reclaiming Important
  - Accumulated impurities require spent solvent disposition
  - Reclaiming concentrates impurities to facilitate environmentally acceptable disposal
  - Reclaiming recycles useful solvent
  - Reclaiming reduces cost of solvent disposition
    - Less material to dispose of
    - Less makeup of fresh amine

# Outline

- Methods
- Impurities to be Reclaimed
- Economic Evaluation of Reclaiming
- Classification of Reclaimer Wastes
- Conclusions

# Reference Cases

Coal – 900 MW, Gas – 810 MW

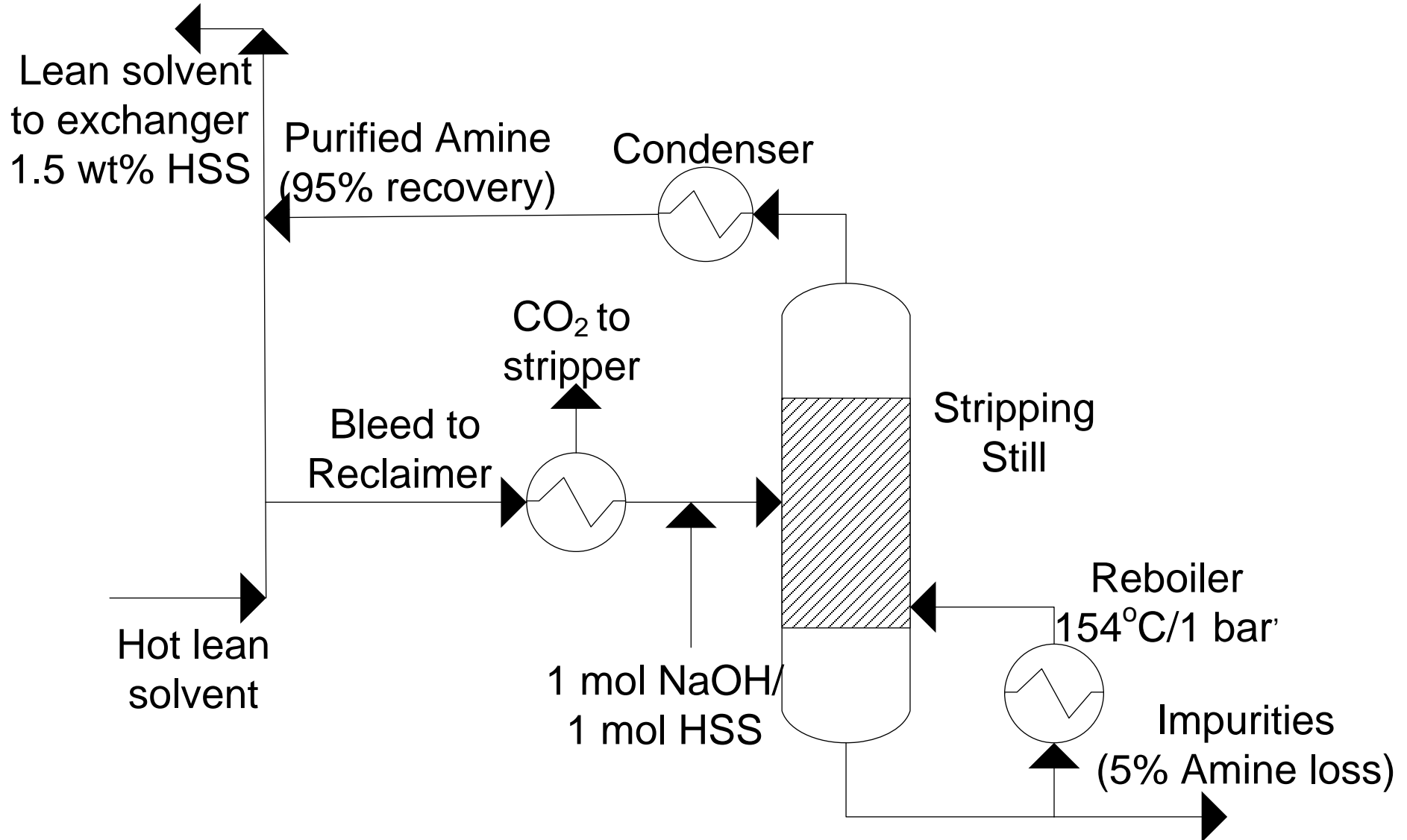
Solvent (Regen T)	Flue Gas	CO <sub>2</sub> Gas (mol %)	CO <sub>2</sub> Loading (mol/mol total alkalinity)		Solvent (standard 1000 m <sup>3</sup> /h)
			Lean	Rich	
7 m MEA (120°C)	Coal	11.8	0.12	0.51	10.7
	Natural Gas	4.1	0.12	0.49	5.1
8 m PZ (150°C)	Coal	11.8	0.31	0.41	21.6
	Natural Gas	4.1	0.28	0.37	10.8
7 m MDEA /2 m PZ (135°C)	Coal	11.8	0.11	0.25	26.7
	Natural Gas	4.1	0.11	0.25	12.1

# Material Balance Assumptions

Reclaiming Technology	Amine Recovery, wt%	HSS removal, wt%	Metals/Non-ionic products removal, wt%
Thermal Reclaiming	95	100	100
Ion Exchange	99	90	0
Electrodialysis	97	91.5	0

Reclaimer bleed adjusted  
to get 1.5% nonvolatile solids in the solvent

# Thermal Reclaiming



# Major impurities with removal of 4.5 ppm SO<sub>2</sub>

## Generation rate

	PZ/Coal	MEA/Coal
	mmol/ kmol CO <sub>2</sub>	mmol/ kmol CO <sub>2</sub>
<b>Nitrosamines (1.5 ppmv NO<sub>2</sub>)</b>	14	7.1
<b>Ammonia</b>	45	37
<b>Total formate</b>	11	6.9
<b>Nonvolatile amines</b>	4.1	11
<b>Volatile amines</b>	5.7	21
<b>Sulfate (4.5 ppmv SO<sub>2</sub>)</b>	42	42
<b>Nitrate (4.5 ppmv NO<sub>x</sub>)</b>	42	42
<b>Chloride (1.8 ppmv HCl)</b>	17	17

# Amine Loss Rate with removal of 4.5 ppm SO<sub>2</sub>

	PZ/Coal	MEA/Coal
	mmol/ kmol CO <sub>2</sub>	mmol/ kmol CO <sub>2</sub>
<b>Total Amine loss</b>	194	221
Thermal degradation	10	24
Oxidation (5 kPa O <sub>2</sub> )	28	56
Nitrosamine (1.5 ppmv NO <sub>2</sub> )	14	7.1
Volatility (1 ppmv emitted)	8	8
Reclaimer loss (95% recovery)	132	124
<b>Amine makeup (\$/MT CO<sub>2</sub>)</b>	<b>\$1.80/MT CO<sub>2</sub></b>	<b>\$0.55/MT CO<sub>2</sub></b>



# Amine loss with better performance of prescrubber

## Removal of 0.5 ppm SO<sub>2</sub> & NO in amine scrubber

	PZ/Coal	MEA/Coal
	mmol/ kmol CO <sub>2</sub>	mmol/ kmol CO <sub>2</sub>
<b>Amine loss</b>	78	129
Thermal degradation	10	24
Oxidation (5 kPa O <sub>2</sub> )	28	56
Nitrosamines (0.5 ppmv NO <sub>2</sub> )	4.8	2.4
Volatility (1 ppmv emitted)	8	8
Reclaimer loss (95% recovery)	27	39
<b>Amine makeup cost</b>	<b>\$0.77/MT CO<sub>2</sub></b>	<b>\$0.33/MT CO<sub>2</sub></b>
<b>(with 4.5 ppm SO<sub>2</sub>)</b>	<b>\$1.80/MT CO<sub>2</sub></b>	<b>\$0.55/MT CO<sub>2</sub></b>

# Estimated Costs of Thermal Reclaiming (Not including disposal) (\$/ton CO<sub>2</sub> captured)

	Amine makeup etc.	Energy	Annualized Capital	Total
MEA Coal	0.53	0.18	0.17	0.90
MEA NGCC	0.38	0.11	0.11	0.60
PZ Coal	1.43	0.17	0.18	1.79
PZ NGCC	0.94	0.11	0.11	1.16

# Costs of Reclaiming PZ w coal (\$/ton CO<sub>2</sub> captured)

	<b>amine makeup etc.</b>	<b>Energy</b>	<b>Annualized Capital</b>	<b>Total</b>
Thermal	1.4	0.17	0.18	1.8
Ion Exchange	1.0	0.00	0.25	1.3
Electrodialysis	1.2	0.22	0.20	1.6

# Qualitative Analysis of Reclaiming Options

- Thermal Reclaiming
  - Removes non-volatile impurities
  - Corrosion is an operational concern
  - Solvent losses are high with expensive solvents
- Ion Exchange
  - Does not remove non-ionic species or transition metals
  - Metals may foul media
  - Large volumes of wastewater
  - Minimal solvent losses
  - Minimal operator attention and maintenance
- Electrodialysis
  - Like ion exchange, but more operator attention
  - Greater solvent losses than ion exchange

# Steady-state toxic impurities (ppm<sub>w</sub>)

## Reclaimed to 1.5 wt% nonvolatiles

Component (ppmw)	7 m MEA		8 m PZ	
	Coal	NGCC	Coal	NGCC
Mercury	0.36	0	0.32	0
Selenium	0.46	0	0.42	0
Chromium	0.91	3.3	0.82	3.8
Nitrosamines	60	60	118	104

Metals in thermal reclaimer waste (coal)  
possibly “Hazardous” in the USA  
may be “Hazardous Waste Generator”

(ppmv)	TC limit	Solvent	Reclaimer	
			Total	Leachate (total/20)
Cr	5	0.90	21.6	1.1
Se	1	0.46	11.0	0.55
Hg	0.2	0.36	8.6	0.43

# In EU, all thermal reclaimer wastes are likely “Hazardous”

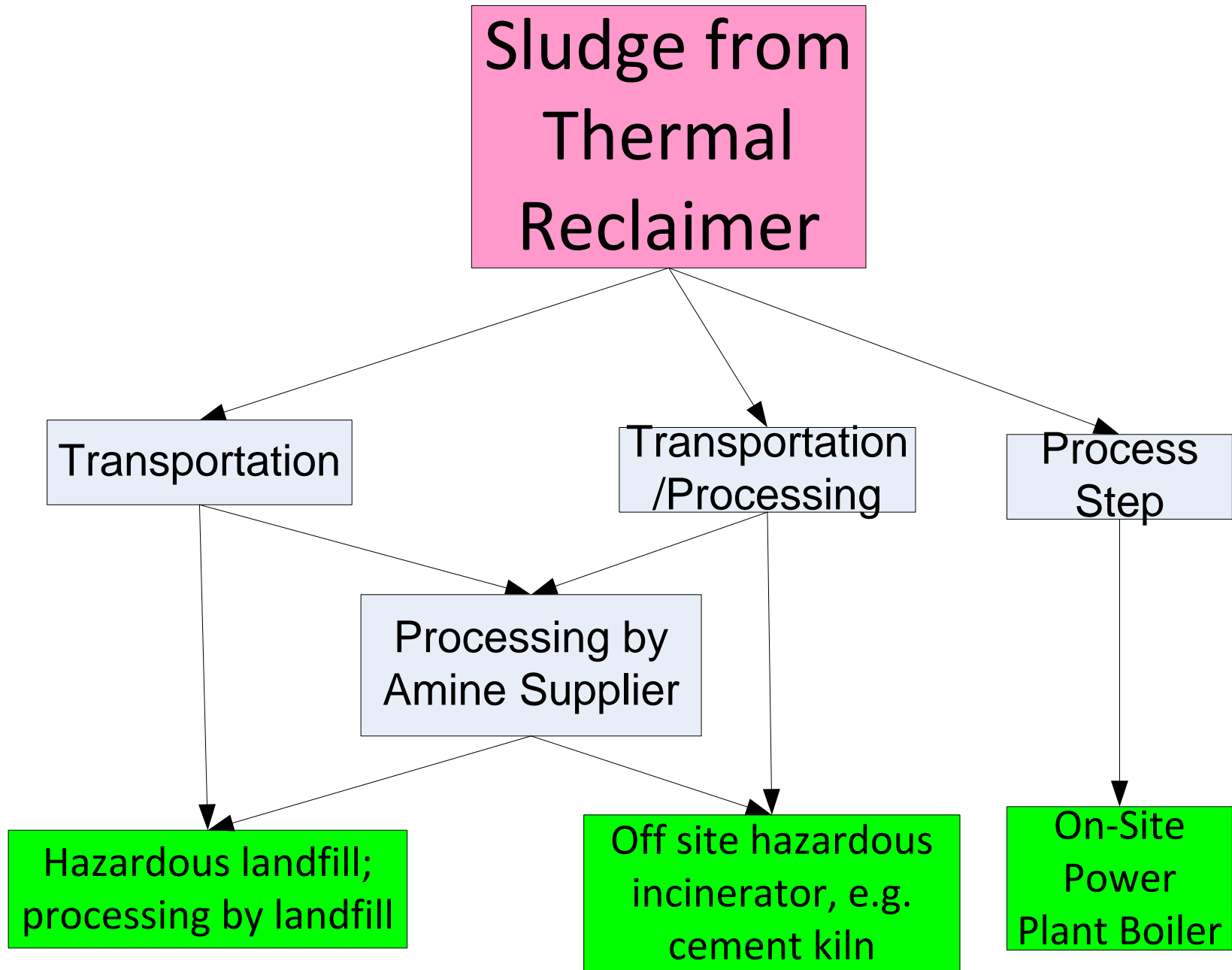
- Solvents in the reclaimer waste are hazardous
  - Irritant
  - Harmful
  - Corrosive
- Metals in reclaimer waste are hazardous
  - Ecotoxicity
  - Listed waste
- PZ containing wastes may add issues with
  - Carcinogenicity (nitrosamines)
  - Sensitizing
  - Perceived Reproductive Toxicity

# Ion Exchange & Electrodialysis Probably Non-hazardous

- Low solvent concentration < thresholds for irritant, harmful, toxic, etc.
- No minimum threshold for sensitizing components, so PZ wastes may be hazardous
- If metals are removed, then waste streams could be listed hazardous wastes



# Disposition Options for Hazardous Waste



# Costs of Disposal

Disposition Option	Reclaiming Case	Annual Cost Added
Non-hazardous landfill	NGCC (US)	15 - 30%
Hazardous landfill or incineration	Coal (US)	~ 100%

# Conclusions

- Cost of reclaiming and solvent makeup will be less than \$2/MT CO<sub>2</sub>, but disposal could make it \$4/MT CO<sub>2</sub>.
- When reclaiming bleed is set by sulfate, etc., Even if more stable, expensive solvent solvents will be less attractive.
- Thermal reclaimer waste will possibly be “hazardous”
  - U.S.: Cr, Se, or Hg.
  - Europe: amine, nitrosamine, metals

# Conclusions

- The uncertainties in cost, quantities, and environmental impact of solvent degradation and reclaiming are large & require additional research.

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